Amendments to the Claims:

This listing of claims will replace all prior versions, and listings, of claims in the application.

Listing of Claims:

1-29. Cancelled

30. (previously presented) A process for producing linear alkyl benzene and linear paraffins, the process including the steps of obtaining a hydrocarbon condensate containing olefins, paraffins and oxygenates from a low temperature Fischer-Tropsch reaction;

a) fractionating a desired carbon number distribution from the hydrocarbon condensate to form a fractionated hydrocarbon condensate stream which is the product of a Fischer-Tropsch reaction;

b) extracting oxygenates from the fractionated hydrocarbon condensate stream from step a) to form a stream containing olefins and paraffins which is the product of a Fischer-Tropsch reaction;

c) alkylating the stream containing olefins and paraffins from step b), which is the product of a Fischer-Tropsch reaction, with benzene in the presence of a suitable alkylation catalyst; and

d) recovering linear alkyl benzene and linear paraffin.

31. (previously presented) The process according to claim 30, wherein, in the extraction step b), the olefin/paraffin ratio of the stream is substantially preserved.

32. (previously presented) The process according to claim 30, wherein the low temperature Fischer-Tropsch reaction is carried out at a temperature of 160°C -

280°C to provide a hydrocarbon condensate containing 60 to 80% by weight paraffins and 10 to 30% by weight olefins.

33. (previously presented) The process according to claim 32, wherein the Fischer-Tropsch reaction is carried out at a temperature of 210°C - 260°C.

34. (previously presented) The process according to claim 32, wherein the Fischer-Tropsch reaction is carried out in the presence of a cobalt catalyst.

35. (previously presented) The process according to claim 32, wherein the hydrocarbon condensate contains less than 25% by weight olefins.

36. (previously presented) The process according to claim 32, wherein the olefins in the hydrocarbon condensate have a degree of linearity of greater than 95%.

37. (previously presented) The process according to claim 36, wherein the paraffins in the hydrocarbon condensate have a degree of linearity of greater than 92%.

38. (previously presented) The process according to claim 30, wherein the hydrocarbon condensate is fractionated, in step a), into the C_8 to C_{16} range.

39. (previously presented) The process according to claim 38, wherein the hydrocarbon condensate product is fractionated, in step a), into the C_{10} to C_{13} range.

40. (previously presented) The process according to claim 39, wherein the fractionated hydrocarbon product contains 10 to 30% by weight olefins with a degree of linearity greater than 92%.

41. (previously presented) The process according to claim 30, wherein the oxygenates are extracted, in step b), by distillation, liquid-liquid extraction or dehydration.

42. (previously presented) The process according to claim 41, wherein the oxygenates are extracted by liquid-liquid extraction.

43. (previously presented) The process according to claim 42, wherein a light solvent is used in the liquid-liquid extraction.

44. (previously presented) The process according claim 43, wherein the light solvent is a mixture of methanol and water.

45. (previously presented) The process according to claim 44, wherein the oxygenate extraction process is a liquid-liquid extraction process that takes place in an extraction column using a mixture of methanol and water as the solvent, wherein an extract from the liquid-liquid extraction is sent to a solvent recovery column from which a tops product comprising methanol, olefins and paraffins is recycled to the extraction column, thereby enhancing the overall recovery of olefins and paraffins.

46. (previously presented) The process according to claim 45, wherein a bottoms product from the solvent recovery column is recycled to the extraction column.

47. (previously presented) The process according to claim 44, wherein the solvent has a water content of more than 3% by weight.

48. (previously presented) The process according to claim 47, wherein the solvent has a water content of from 5% - 15% by weight.

49. (previously presented) The process according to claim 45, wherein a raffinate from the extraction column is sent to a stripper column from which a hydrocarbon stream containing more than 90% by weight olefins and paraffins and less than 0.2% by weight oxygenates exits as a bottoms product.

50. (previously presented) The process according to claim 49, wherein the bottoms product contains less than 0.02% by weight oxygenates.

51. (previously presented) The process according to claim 30, wherein the recovery of olefins and paraffins in the hydrocarbon feed stream over the extraction step b) is in excess of 70%.

52. (previously presented) The process according to claim 51, wherein the recovery of olefins and paraffins is in excess of 80%.

53. (previously presented) The process according to claim 30, wherein the olefin/paraffin ratio of the fractionated hydrocarbon condensate stream a) is substantially preserved over the extraction step b).

54. (previously presented) The process according to claim 30, wherein the alkylation catalyst in step c) is a solid acid catalyst.

55. (previously presented) A fractionated hydrocarbon condensate product from a Fischer-Tropsch reaction, in the C_8 to C_{16} range, containing olefins with a degree of linearity of greater than 92%, and less that 0.015% by weight oxygenates, for use in a process for manufacturing linear alkyl benzene.

56. (previously presented) The fractionated hydrocarbon condensate product according to claim 55 in the C_{10} to C_{13} range.

57. (previously presented) The fractionated hydrocarbon condensate according to claim 55, wherein the olefins have a degree of linearity of greater than 95%.

58. (previously presented) A linear alkyl benzene product formed by an alkylation process of olefins, said olefins being a product of a Fischer-Tropsch reaction, wherein the linear alkyl benzene product has a degree of linearity of greater than 90%.

59. (previously presented) The linear alkyl benzene product according to claim 58, having a degree of linearity of greater than 94%.